

AMENDMENTS TO THE CLAIMS:

This listing of claims will replace all prior versions and listings of claims in the application:

1. (Currently amended) Process for the gas-phase ~~(co-)polymerisation~~ (co-)polymerization of olefins in a ~~fluidised~~ fluidized bed reactor using a Ziegler-Natta type catalyst, said process comprising the addition into the reactor of an organoaluminium cocatalyst and of a monohalogenated hydrocarbon compound,
 - a. wherein the molar ratio of the monohalogenated hydrocarbon compound to the cocatalyst is comprised between 0.02 and 0.2, ~~preferably between 0.02 and 0.15,~~
 - b. wherein the monohalogenated hydrocarbon compound is added to the reactor in an amount comprised between 0.1 to 40 moles of monohalogenated hydrocarbon compound per mole of transition metal of catalyst introduced into the reactor, ~~preferably in a mole ratio comprised between 0.2 and 40, preferably 0.2 and 10, more preferably 0.25 and 5, and~~
 - c. wherein the monohalogenated hydrocarbon compound is n-butyl chloride.
2. (Currently amended) Process according to ~~the preceding claims~~ claim 1 wherein the Ziegler-Natta type catalyst is a silica supported Ziegler-Natta catalyst.
3. (Currently amended) Process according to ~~the preceding claims~~ claim 1 or 2, wherein the molar ratio of the monohalogenated hydrocarbon compound to the cocatalyst is maintained constant throughout the ~~polymerisation~~ polymerization.
4. (Currently amended) Process according to ~~any of the preceding claims~~ claim 1, wherein the sole or main olefin is either ethylene or propylene, and the

optional comonomer is selected from but-1-ene, pent-1-ene, hex-1-ene, 4-methylpent-1-ene and oct-1-ene.

5. (Currently amended) Process according to ~~any of the preceding claims~~ claim 1, wherein the monohalogenated hydrocarbon compound is diluted in a ~~conventional diluent like butane, pentane or hexane~~ in an amount comprised between 0.001 and 2 mole of monohalogenated hydrocarbon compound per 1 of diluent.

6. (Currently amended) Process according to ~~any of the preceding claims~~ claim 1, wherein the monohalogenated hydrocarbon compound is not added in admixture with the catalyst.

7. (Currently amended) Process according to ~~any of the preceding claims~~ claim 1, wherein the catalyst is a non-prepolymerized catalyst.

8. (Currently amended) Process according to claim 7, wherein the catalyst is a titanium magnesium silica supported catalyst which is directly introduced into the reactor.

9. (New) Process according to claim 1, wherein the cocatalyst is comprised between 0.02 and 0.15.

10. (New) Process according to claim 1, wherein the amount in b. is between 0.2 and 40.

11. (New) Process according to claim 10, wherein the amount in b. is between 0.2 and 10.

12. (New) Process according to claim 11, wherein the amount in b. is between 0.25 and 5.

13. (New) Process according to claim 5, wherein the diluent is selected from the group consisting of butane, pentane and hexane.